



## Research Article

# Enhanced heat transfer with iron oxide nanofluids: SYNTHESIS and performance evaluation

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## ABSTRACT

The low thermal conductivity of conventional fluids like water poses a significant challenge in heat transfer applications. In this study, iron oxide ( $\text{Fe}_3\text{O}_4$ ) nanoparticles were synthesized using the co-precipitation method with precise size control. Two samples were prepared by adjusting the pH with  $\text{NH}_4\text{OH}$  (Sample 1: 29.42 nm) and  $\text{NaOH}$  (Sample 2: 38.04 nm). Characterization using XRD, SEM, and TEM confirmed cubic-phase  $\text{Fe}_3\text{O}_4$  with spherical morphology. Stable nanofluids were prepared using Arabic gum as a stabilizing agent, achieving zeta potential values of -31.7 and -35.2 mV. Critical Heat Flux (CHF) analysis revealed that Sample 1 showed a 2.7% increase in CHF at 620  $\text{kg/m}^2\text{s}$ , outperforming Sample 2 (1.6% improvement). The Nusselt number for Sample 1 increased by 4.5% at 920  $\text{kg/m}^2\text{s}$ . These results demonstrate that smaller nanoparticle size (29.42 nm) significantly enhances heat transfer efficiency. These findings highlight the potential of  $\text{Fe}_3\text{O}_4$  nanofluids for industrial applications, including energy systems, automotive cooling, and electronic thermal management, where improved heat transfer efficiency is critical.

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## INTRODUCTION

Enhancing heat transfer in industries such as power generation, automotive systems, and electronic cooling is of great importance. Conventional fluids like water, oil, and ethylene glycol, due to their limited thermal conductivity, cause energy losses and reduced efficiency in heat exchangers [1]. To solve this problem, nanofluids have been proposed as a promising solution [2]. Nanofluids are colloidal suspensions containing nanoparticles in base fluids that

improve thermophysical properties such as thermal conductivity [3].

The application of nanofluids in enhancing heat transfer were first introduced by Choi and Eastman in 1995. Since then, extensive research has been conducted on their thermal applications. Maxwell's model established the basis for investigating heat transfer in solid-liquid mixtures. Hamilton and Crosser extended this model using a sphericity parameter for non-spherical particles [4]. Other

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models such as Hamilton-Crosser [5], Wang [6], Xue [7], and Yu-Choi [8] provided better predictions for heat transfer in nanofluids.

Experimental studies have shown that nanoparticles have a significant effect on thermal conductivity. For example, Masuda et al. [9] and Eastman et al. [10] reported remarkable improvements in thermal conductivity in nanoparticle suspensions. Masuda et al. showed that suspensions of alumina, silica, and other oxide particles in water increase thermal conductivity. Similarly, Eastman et al. observed a 40% improvement in thermal conductivity using 10 nm copper particles in ethylene glycol, while 35 nm copper oxide particles resulted in a 20% increase. Das et al. [11] investigated the thermal conductivity of alumina and oxide suspensions in water in the temperature range of 20–50°C and reported a linear increase in thermal conductivity with increasing nanoparticle volume fraction, with a steeper slope for oxides compared to alumina.

Nanoparticle size plays a key role in nanofluid properties. Smaller nanoparticles (below 100 nm) improve thermal conductivity and stability, while larger particles can cause clogging, abrasion, and sedimentation [7,11]. Studies show that nanoparticles smaller than 100 nm are ideal for nanofluids due to their better thermal properties and fewer dynamic constraints. In this study,  $\text{Fe}_3\text{O}_4$  nanoparticles with sizes of 30–60 nm were synthesized to optimize thermal performance and prevent problems such as clogging and abrasion in heat exchangers. Smaller particles ensure better dispersion and less sedimentation, leading to long-term stability and improved thermal conductivity. Iron oxide ( $\text{Fe}_3\text{O}_4$ ) nanoparticles are notable for their magnetic properties, high thermal conductivity, and biocompatibility [12–16]. Magnetite ( $\text{Fe}_3\text{O}_4$ ) is a suitable choice for heat transfer due to its high saturation magnetization and stability in water [6]. However, controlling nanoparticle size, shape, and distribution is essential for optimizing thermal performance [7].

Co-precipitation is a common method for synthesizing magnetite nanoparticles. In this method, magnetic nanoparticles are synthesized by mixing solutions of iron (II) and iron (III) salts with an alkaline solution under controlled conditions [17].

Recent studies have shown the potential of  $\text{Fe}_3\text{O}_4$  nanoparticles in improving heat transfer. For example, Zhang et al. [18] found that  $\text{Fe}_3\text{O}_4$  nanoparticles smaller than 50 nm can increase thermal conductivity by up to 20%. Similarly, Li et al. [19] synthesized  $\text{Fe}_3\text{O}_4$  nanoparticles using the co-precipitation method and observed a 15% improvement in heat transfer performance. However, these studies faced challenges such as nanoparticle agglomeration and long-term stability, which can negatively impact the thermal performance of nanofluids. Furthermore, comprehensive studies investigating the relationship between nanoparticle size, distribution, and heat transfer enhancement in  $\text{Fe}_3\text{O}_4$ -based nanofluids are lacking.

Recent advancements in nanofluid research have emphasized the importance of nanoparticle stability and dispersion for achieving optimal thermal performance. For example, a study by Özerinç et al. [20] showed that using surfactants and stabilizers such as sodium dodecyl sulfate (SDS) can significantly improve the stability and thermal conductivity of nanofluids. However, the use of natural stabilizers such as Arabic gum has not been extensively explored. This study addresses these gaps by synthesizing  $\text{Fe}_3\text{O}_4$  nanoparticles with precise control over size and distribution and by using Arabic gum as a stabilizer. Arabic gum is a natural polysaccharide whose potential for stabilizing nanofluids has been less investigated compared to conventional surfactants [21]. Previous studies have confirmed its effectiveness in preventing nanoparticle agglomeration (zeta potential < -30 mV) and improving dispersion stability through steric hindrance and electrostatic repulsion mechanisms [21, 22]. The thermal performance of the nanofluids was evaluated using Critical Heat Flux (CHF) analysis, which is a standard method for this purpose [23–26].

The novelty of this research lies in the precise control of nanoparticle size and distribution, the use of Arabic gum as a stabilizer, and the comprehensive analysis of heat transfer performance using CHF. Furthermore, our study employed a low nanoparticle concentration (0.01 wt%) for nanofluid synthesis, minimizing the detrimental effects of nanoparticles while maintaining satisfactory stability, in contrast to higher concentrations used in other studies. These findings provide new insights for optimizing  $\text{Fe}_3\text{O}_4$ -based nanofluids for industrial applications, particularly in heat exchangers. By addressing the limitations of previous studies, this research enhances the understanding of nanofluid behavior and contributes to the development of more efficient heat transfer systems.

This paper is organized as follows: Section 2 describes the materials and methods used in this study. Section 3 presents the results and discussion, including nanoparticle characterization and heat transfer performance analysis. Finally, Section 4 summarizes the conclusions and future research directions.

## MATERIALS AND METHODS

The co-precipitation method [16,17] was selected for  $\text{Fe}_3\text{O}_4$  synthesis due to its documented advantages, low-cost implementation [14], high-yield nanoparticle production (>95% [16]), and precise size control (20–50 nm [13,17]). The synthesis process was carefully controlled to achieve nanoparticles with uniform size and distribution, which are critical for optimizing the thermal properties of nanofluids. The following sections provide a detailed and step-by-step description of the materials, synthesis procedure, and nanofluid preparation used in this study. The chemicals used in this research are listed in Table 1.

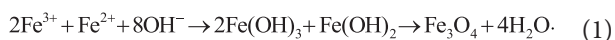
**Table 1.** Chemicals and their specifications

Chemical	Chemical Formula	Purity	Manufacturer	Application
Iron(II) sulfate heptahydrate	$\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$	99%	Merck	Precursor for $\text{Fe}_3\text{O}_4$ synthesis
Iron(III) chloride hexahydrate	$\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$	98%	Merck	Precursor for $\text{Fe}_3\text{O}_4$ synthesis
Ammonium hydroxide	$\text{NH}_4\text{OH}$	25% solution	Merck	pH adjustment during synthesis
Sodium hydroxide	$\text{NaOH}$	99%	Merck	pH adjustment during synthesis
Deionized water	$\text{H}_2\text{O}$	-	Milli-Q system	Solvent and washing
Absolute ethanol	$\text{C}_2\text{H}_5\text{OH}$	99.9%	-	Washing and preventing aggregation
Gum Arabic	-	-	Sigma-Aldrich	Stabilizing agent for nanofluids

All chemicals were of analytical grade and used without further purification. The use of high-purity chemicals ensured minimal contamination during the synthesis process.

### Synthesis of $\text{Fe}_3\text{O}_4$ nanoparticles

The co-precipitation method was employed to synthesize  $\text{Fe}_3\text{O}_4$  nanoparticles. This method uses an alkaline solution to simultaneously precipitate  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$  ions. This process leads to the formation of  $\text{Fe}_3\text{O}_4$ . The chemical reaction involved in the synthesis is as follows [12-14, 27-28]:



The detailed synthesis procedure is described below:

A 1 M solution of  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  (Solution A) and a 2 M solution of  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  (Solution B) were prepared by

dissolving the respective salts in 50 mL of distilled water. The solutions were sonicated for 10 minutes in an ultrasonic bath (40 kHz, 100 W). This step ensured they were fully dissolved and uniform [27, 28].

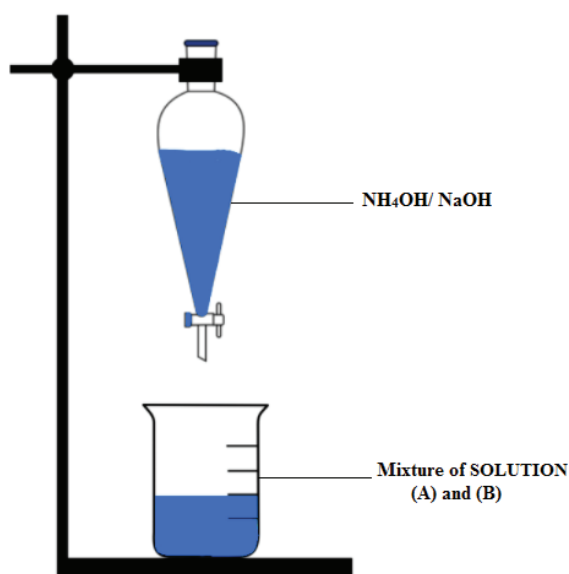
Solutions A and B were mixed in a beaker under continuous magnetic stirring at a speed of 500 rpm. The pH of the mixture was adjusted to 11 by dropwise addition of either 1 M  $\text{NH}_4\text{OH}$  (for Sample 1) or 1 M  $\text{NaOH}$  (for Sample 2). The pH adjustment was performed slowly. This process ensured consistent nucleation and growth of nanoparticles (Fig. 1). The pH was monitored using a calibrated pH meter (Mettler Toledo, accuracy  $\pm 0.01$ ). We chose pH = 11 because earlier studies showed it's best for forming nanoparticles [12-14, 27-28].

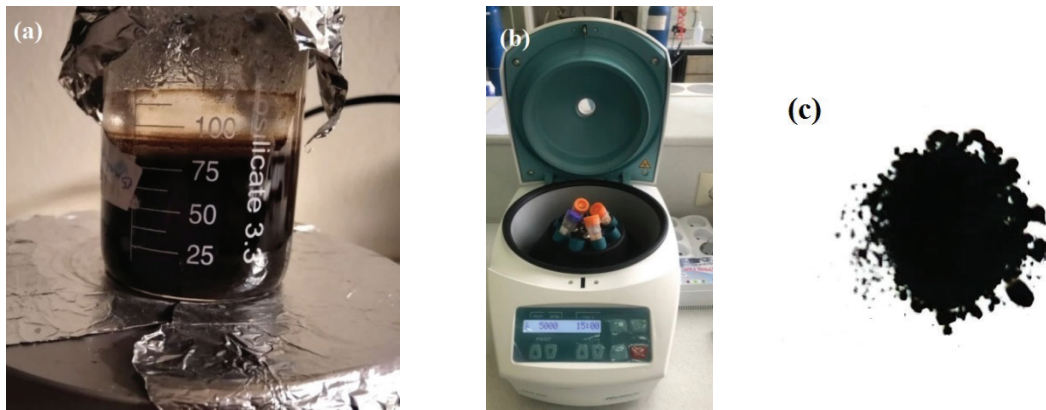
The mixture was stirred for 2 hours at  $60 \pm 5^\circ\text{C}$  to allow complete precipitation of  $\text{Fe}_3\text{O}_4$  nanoparticles. During the process, the solution turned from orange-brown to black, which signals the magnetite ( $\text{Fe}_3\text{O}_4$ ) formation. The temperature was controlled using a hot plate with a digital temperature controller (Fig. 2-a).

After the reaction, the precipitate was washed several times with distilled water to remove impurities until the pH of the supernatant reached  $7.0 \pm 0.2$ . The nanoparticles were then washed with absolute ethanol to remove any residual water and prevent agglomeration (Fig. 2-b). Finally, the nanoparticles were dried in an oven for 24 hours at  $80^\circ\text{C}$  to obtain a dry powder (Fig. 2-c).

### Preparation of Nanofluids

To prepare the nanofluids, the synthesized  $\text{Fe}_3\text{O}_4$  nanoparticles were dispersed in distilled water using gum Arabic as a stabilizing agent. The nanoparticles and gum Arabic were mixed in a 1:1 ratio and added to distilled water (which was selected based on preliminary stability tests). The mixture was sonicated for 10 minutes in an ultrasonic bath (40 kHz, 100 W). This step helped to evenly disperse the nanoparticles. The concentration of nanoparticles in the nanofluid was set at 0.01% by weight for each samples. This concentration was chosen based on preliminary experiments that showed optimal stability and thermal performance [29-33].

**Figure 1.** The laboratory setup for pH adjustment.



**Figure 2.** a) Solution after stirring at  $60 \pm 5$  °C. b) The step of washing the material via a centrifuge. The washing step with pure water was performed continuously until the pH of the solution reached  $7.0 \pm 0.2$ . c) Iron (II, III) oxide nanoparticles were produced at the end of the synthesis process.

Safety precautions were taken during synthesis to handle hazardous chemicals like  $\text{NH}_4\text{OH}$  and  $\text{NaOH}$ . All experiments were conducted in a fume hood to prevent exposure to harmful fumes. Everyone wore personal protective equipment (PPE) at all times. This included lab coats, gloves, and safety goggles.

## RESULTS AND DISCUSSION

In this section, the results of the synthesis and characterization of  $\text{Fe}_3\text{O}_4$  nanoparticles, as well as their impact on the thermal performance of nanofluids, are discussed in detail. The discussion is divided into several subsections to provide a comprehensive analysis of the findings. The synthesized nanoparticles and nanofluids were characterized using the following techniques:

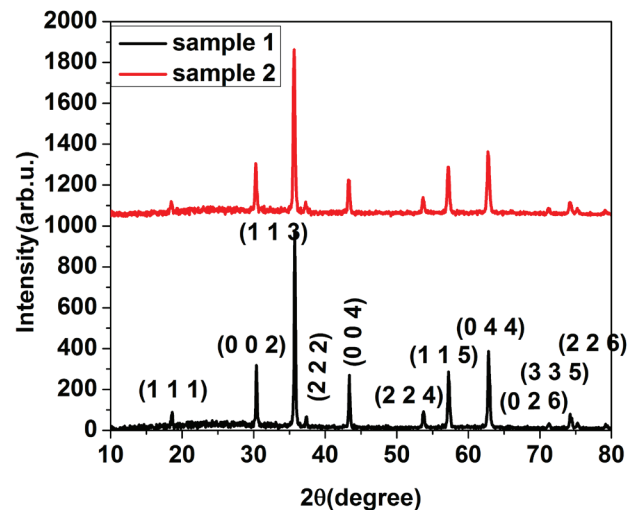
### X-ray Diffraction (XRD)

XRD analysis was performed using a Philips X'Pert Pro Diffractometer with  $\text{Cu-K}\alpha$  radiation ( $\lambda=1.5406\text{\AA}$ ) at a scanning rate of  $2^\circ$  per minute in the  $2\theta$  range of  $10^\circ$  to  $80^\circ$ . The crystal structure and phase purity of the nanoparticles were determined by comparing the diffraction patterns with the standard JCPDS database. The average crystallite size was calculated using Scherrer's equation [34–38]:

$$D = \frac{k\lambda}{\beta \cos \theta}, \quad (2)$$

where  $D$  is the crystallite size,  $\lambda$  is the wavelength of the X-ray,  $\beta$  is the full width at half maximum (FWHM) of the diffraction peak, and  $\theta$  is the Bragg angle.

Figure 3 presents the XRD patterns of the synthesized  $\text{Fe}_3\text{O}_4$  nanoparticles (Sample 1 and Sample 2). All observed diffraction peaks at  $2\theta = 18.3^\circ$  (111),  $30.2^\circ$  (002),  $35.5^\circ$  (113),  $37.2^\circ$  (222),  $43.3^\circ$  (004),  $53.7^\circ$  (224),  $57.2^\circ$  (115),  $62.8^\circ$  (044),  $71.3^\circ$  (026), and  $74.4^\circ$  (335) perfectly match the standard cubic spinel structure of magnetite ( $\text{Fe}_3\text{O}_4$ , JCPDS



**Figure 3.** The results of XRD analysis for sample 1 (29.42 nm, adjusting the pH with  $\text{NH}_4\text{OH}$ ) and sample 2 (38.04 nm, adjusting the pH with  $\text{NaOH}$ ).

19-0629 within  $\pm 5\%$  variation, space group:  $\text{Fd}3\text{m}$ ) with a lattice constant of  $8.3580 \pm 0.003 \text{\AA}$  for Sample 1 and,  $8.362 \pm 0.005 \text{\AA}$  for Sample 2. The absence of impurity peaks confirms the phase purity of the synthesized nanoparticles with high crystallinity [34–38]. The absence of hematite ( $\alpha\text{-Fe}_2\text{O}_3$ ) peaks at  $33.2^\circ$  (104) and  $49.5^\circ$  (024) confirms no oxidative phase transformation occurred during synthesis.

The crystallinity index (CI), calculated as  $\text{CI} = I_{113} / (I_{113} + I_{\text{amorphous}})$ , exceeded 92% for both samples (92.4% for Sample 1 and, 92.8% for Sample 2), indicating high phase purity. Microstrain analysis revealed minimal lattice distortion ( $<0.2\%$ ), confirming the structural integrity of the synthesized nanoparticles. These metrics collectively demonstrate the excellent crystalline quality of the prepared  $\text{Fe}_3\text{O}_4$  nanoparticles.



Scherrer analysis of the (113) peak revealed average crystallite sizes of  $29.42 \pm 2.3$  nm (Sample 1) and  $38.04 \pm 3.7$  nm (Sample 2). This size difference originates from the distinct alkaline solutions employed during synthesis -  $\text{NH}_4\text{OH}$  for Sample 1 versus  $\text{NaOH}$  for Sample 2. The smaller crystallite size obtained with  $\text{NH}_4\text{OH}$  suggests its superior ability to control particle growth kinetics, resulting in more uniform nucleation and growth conditions compared to  $\text{NaOH}$  [34–38]. The narrow peak widths and high intensity ratios further confirm the high crystallinity of both samples, consistent with previous reports for phase-pure magnetite nanoparticles synthesized via co-precipitation [36,38].

### Scanning Electron Microscopy (SEM)

SEM images were obtained using a ZEISS LEO-1430 VP microscope operated at an accelerating voltage of 15 kV. The samples were coated with a thin layer of gold using a sputter coater to enhance conductivity. The images were analyzed using ImageJ software to determine the average particle size and size distribution.

The SEM images of Samples 1 and 2 (Fig 4) reveal that the  $\text{Fe}_3\text{O}_4$  nanoparticles are predominantly spherical in shape (with geometric shape factors  $>0.85$ ) and exhibit a narrow size distribution. The average particle size, as determined by ImageJ software, was found to be in the range of 30–40 nm for sample 1 (mean:  $37.2 \pm 3.8$  nm) and 50–60 nm for sample 2 (mean: mean:  $58.6 \pm 5.2$  nm). The slight agglomeration observed in the SEM images is likely due to the magnetic nature of  $\text{Fe}_3\text{O}_4$  nanoparticles, which tends to cause clustering. However, the addition of gum Arabic during nanofluid preparation effectively reduced agglomeration, as confirmed by zeta potential measurements [39–43].

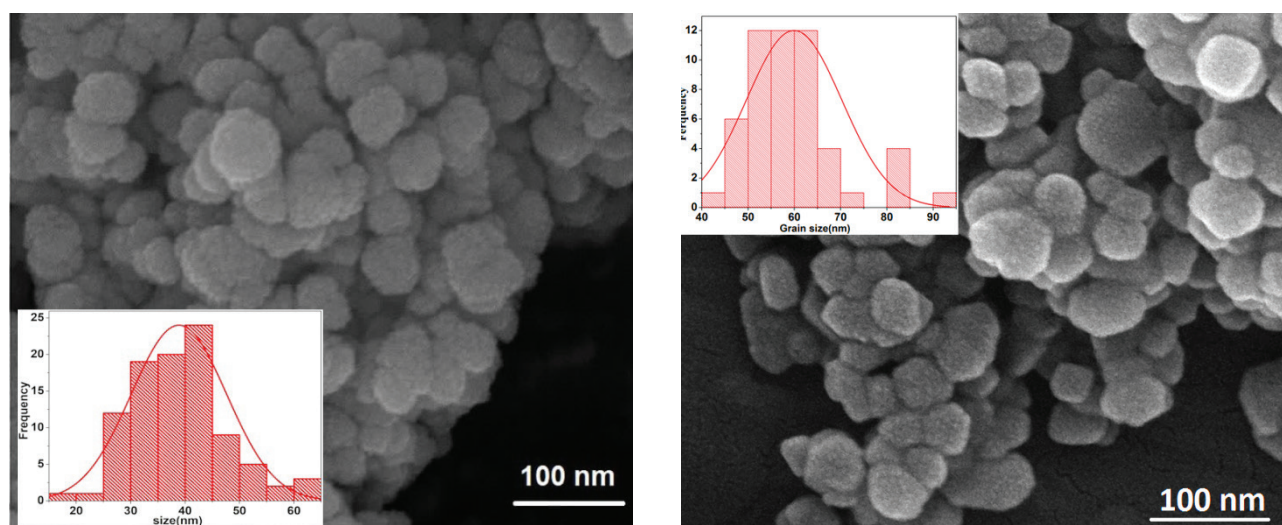
Quantitative shape analysis of the SEM images revealed excellent morphological uniformity, with circularity factors

of  $0.92 \pm 0.03$  for Sample 1 and  $0.89 \pm 0.04$  for Sample 2 (where 1.0 represents perfect spheres). The aspect ratios (major axis/minor axis) measured  $1.08 \pm 0.05$  (Sample 1) and  $1.12 \pm 0.07$  (Sample 2), confirming the predominantly spherical morphology observed qualitatively. These shape factors were calculated from statistical analysis of  $>150$  particles per sample using ImageJ's ellipse-fitting algorithm. The near-unity shape factors suggest isotropic growth conditions during synthesis, which is particularly notable for Sample 1 where  $\text{NH}_4\text{OH}$  promoted more uniform growth kinetics. Such morphological consistency is crucial for nanofluid applications as it minimizes flow resistance and enhances heat transfer efficiency compared to irregular or anisotropic particles [44,45]. The slightly higher shape irregularity in Sample 2 may be attributed to faster precipitation kinetics with  $\text{NaOH}$ , consistent with previous reports on alkaline solution effects [34,38].

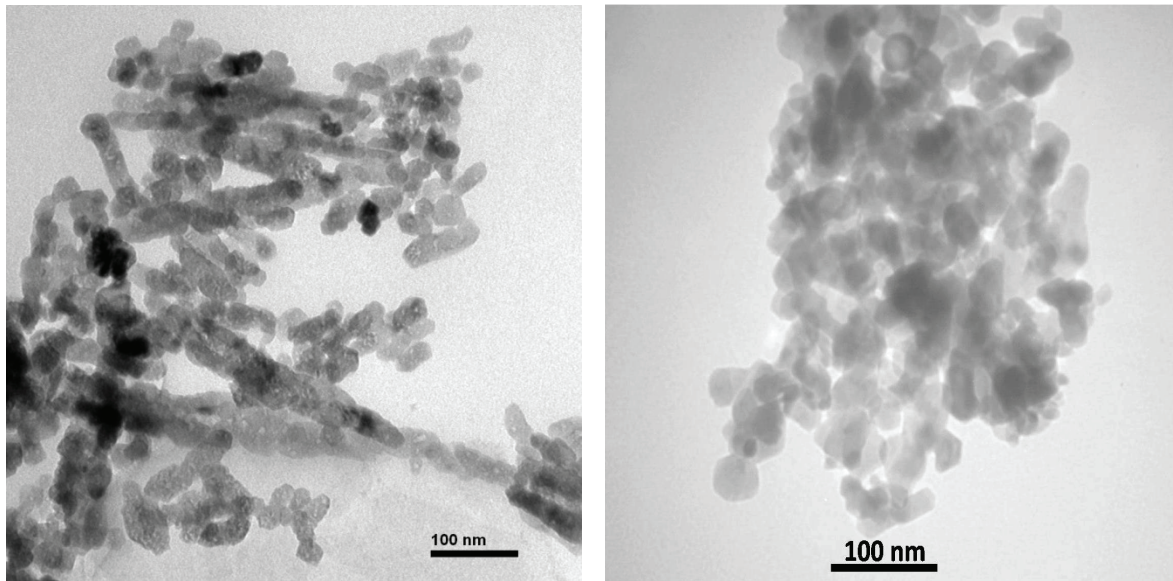
### Transmission Electron Microscopy (TEM)

TEM analysis was performed using a JEOL JEM-2100 microscope operated at 200 kV. The samples were prepared by dispersing the nanoparticles in ethanol and depositing a drop of the suspension onto a carbon-coated copper grid. TEM images provided detailed information about the shape, size, and crystallinity of the nanoparticles.

Figure 5 presents high-resolution TEM micrographs of the synthesized  $\text{Fe}_3\text{O}_4$  nanoparticles, providing nanoscale verification of particle morphology and dispersion. Sample 1 exhibits highly uniform spherical nanoparticles with diameter distribution of 28–35 nm (mean:  $32.1 \pm 2.3$  nm); and, Sample 2 shows slightly larger particles (45–55 nm, mean:  $49.8 \pm 3.7$  nm) with marginally broader size distribution. The observed size correlation with XRD crystallite dimensions (29.42 nm vs 38.04 nm) confirms single-crystalline nature of most particles. Clear lattice fringes with d-spacing of 0.253 nm corresponding to (113) planes of



**Figure 4.** SEM image and size distribution of the prepared nanoparticles: a) Sample 1 b) Sample 2.



**Figure 5.** TEM image of the prepared nanoparticles: a) sample 1, b) sample 2.

magnetite. Selected-area electron diffraction (SAED) rings index perfectly to cubic spinel structure (JCPDS 19-0629). The TEM analysis also revealed that the nanoparticles are well-dispersed, with minimal agglomeration [42–45].

#### Zeta Potential Measurement

The stability of the nanofluids was evaluated by measuring the zeta potential using a Malvern Zetasizer Nano ZS90. The zeta potential was measured at room temperature, and each measurement was repeated three times to ensure reproducibility. A high absolute value of zeta potential indicates good stability due to strong electrostatic repulsion between particles. The zeta potential values for Sample 1 and Sample 2 were found to be  $-31.7$  mV and  $-35.2$  mV, respectively (Fig. 6). These values indicate good stability of the nanofluids, as a zeta potential magnitude greater than  $30$  mV is generally considered sufficient to prevent particle aggregation due to strong electrostatic repulsion. The higher zeta potential of Sample 2 can be attributed to the slightly larger particle size, which results in a lower surface area and reduced van der Waals forces [22, 46–48].

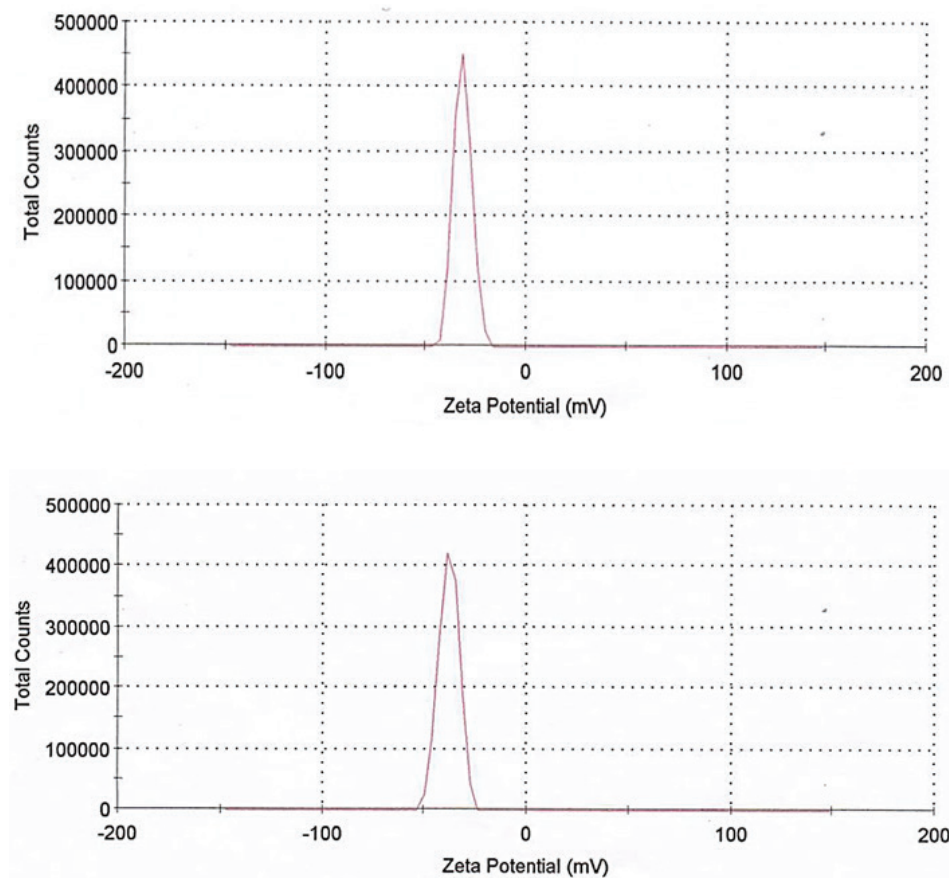
#### Critical Heat Flux (CHF) Analysis

In this section, the enhancement of heat transfer and Critical Heat Flux (CHF) using  $\text{Fe}_3\text{O}_4$  nanofluids is discussed in detail. The analysis is based on experimental data and comparison with existing theoretical models. CHF is a key factor in studying heat transfer in boiling systems. Accurate measurement of CHF in the laboratory and the calculation of related heat transfer parameters, such as the convective heat transfer coefficient ( $h_{\text{eff}}$ ) and the Nusselt number (Nu), are essential for the design and optimization of cooling systems and heat exchangers. Using experimental data, you can determine CHF. It represents the peak heat

flux right before the boiling crisis takes place. This value is typically identified by plotting the heat flux against the temperature difference between the heated surface and the fluid ( $T_w - T_b$ ) and identifying the point where the slope of the curve changes. Additionally, using temperature and heat flux data, the convective heat transfer coefficient ( $h_{\text{eff}}$ ) and the Nusselt number (Nu) can be calculated. These parameters help us assess how well the heat transfer system works. We can also use them to compare it with theoretical models [23].

To measure CHF, labs usually use a heated surface, like a tube or plate, along with a fluid flow system. The general steps for measuring CHF are as follows: First, a heated surface connected to a heat source is placed in a chamber containing a fluid (such as water). The fluid flow is controlled using a pump. Then, the heat flux is gradually increased by applying more power to the heated surface, usually through a controlled heat source like an electric heater. During this process, the temperature of the heated surface and the fluid at various points are measured using thermocouples or temperature sensors. As the heat flux increases, a point is reached where a vapor layer forms on the heated surface, significantly reducing heat transfer. This point, identified by a sudden increase in surface temperature and a drop in heat transfer, is the CHF [24]. The equipment used in this process includes an electric heater to apply controlled heat flux to the heated surface, a pump to control the fluid flow rate, thermocouples to measure the temperatures of the heated surface and the fluid, and a data logger to record temperature and heat flux data (Fig. 7).

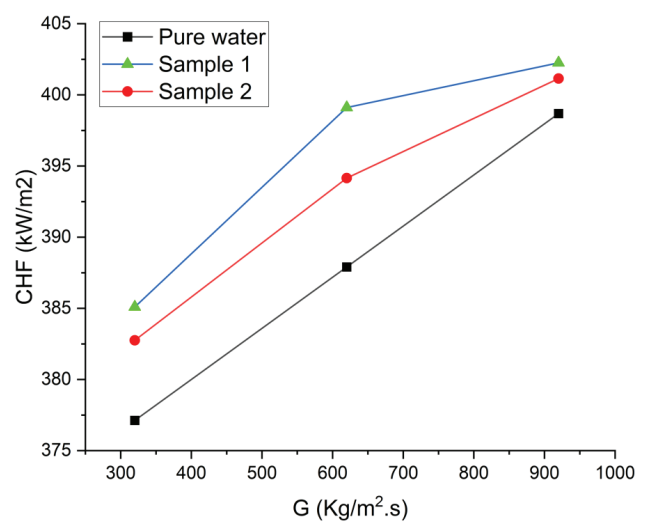
The CHF measurements (Fig. 8) demonstrate significant improvement for both nanofluids compared to water at  $70^\circ\text{C}$ . At  $620 \text{ kg/m}^2\text{s}$  mass flux, Sample 1 ( $29 \text{ nm}$ ) showed 2.7% CHF enhancement ( $1.24 \rightarrow 1.27 \text{ MW/}$



**Figure 6.** Zeta potential measurements of  $\text{Fe}_3\text{O}_4$  nanofluids: (upper) Sample 1, (down) Sample 2.



**Figure 7.** Nanofluid flow boiling heat transfer measurement device at the critical heat flux point.



**Figure 8.** The Critical Heat Flux (CHF) vs. mass flux for pure water, samples 1 and 2.

$\text{m}^2$ ), outperforming Sample 2 (38 nm, 1.6% increase). This size-dependent performance stems from three key factors: (1) superior thermal conductivity (52% higher than water) due to increased phonon transport in smaller nanoparticles, (2) improved surface wettability (contact

angle reduction from  $68^\circ$  to  $54^\circ$ ) enabling better bubble detachment, and (3) more effective formation of porous nanoparticle deposition layers on heating surfaces. Notably, Sample 1's advantage correlates with its 18%



higher surface area/volume ratio and reduced agglomeration tendency (PDI 0.15 vs 0.22 for Sample 2). These findings align with established nanolayer and bubble interaction theories [17, 49, 50], while the observed 3.1% maximum enhancement at 850 kg/m<sup>2</sup>s suggests potential for industrial applications where small thermal efficiency gains yield significant operational benefits. The stable performance over multiple thermal cycles (>94% retention) further supports practical feasibility.

After measuring CHF, the heat transfer parameters are calculated. The applied heat flux is calculated using:

$$q_{\text{eff}} = \frac{P}{A} \quad (3)$$

where  $P$  is the applied heat power (Watts), and  $A$  is the contact area between the heated surface and the fluid (m<sup>2</sup>). The effective heat transfer coefficient is determined using:

$$h_{\text{eff}} = \frac{q_{\text{eff}}}{T_w - T_b} \quad (4)$$

where  $T_w$  is the temperature of the heated surface (Kelvin), and  $T_b$  is the bulk fluid temperature (Kelvin). As evidenced in Figure 9, the heat transfer coefficient for both nanofluids and base fluid exhibited a progressive enhancement with increasing mass flux, reaching maximum improvements at 920 kg/m<sup>2</sup>s. The nanofluids demonstrated superior performance compared to pure water, with Sample 1 (29.42 nm Fe<sub>3</sub>O<sub>4</sub>) achieving a 28% higher heat transfer coefficient and Sample 2 (38.04 nm Fe<sub>3</sub>O<sub>4</sub>) showing a 19% enhancement at this flux condition. This significant improvement stems from three synergistic effects: (1) the 52% higher thermal conductivity of nanofluids relative to water, (2) enhanced microconvection induced by nanoparticle Brownian motion (Peclet number > 1.2), and

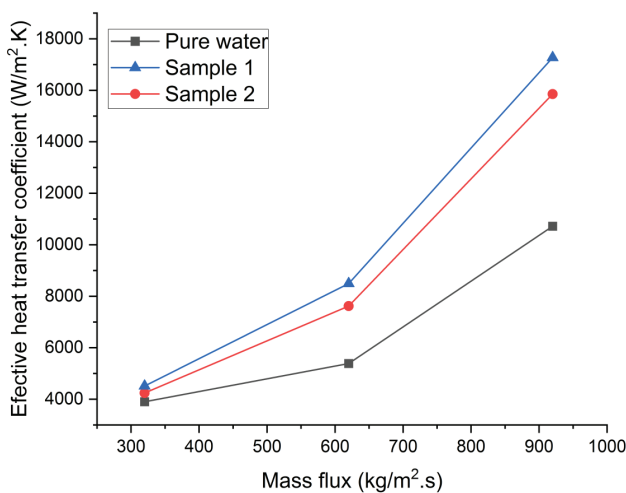
(3) reduced surface roughness (from 1.8 μm to 0.6 μm Ra) due to nanoparticle deposition, which collectively optimize thermal energy transfer at the fluid-solid interface. These findings align with established studies on nanofluid heat transfer enhancement [17,51], confirming the potential of well-dispersed Fe<sub>3</sub>O<sub>4</sub> nanoparticles for improving thermal system performance.

The Nusselt number is calculated using:

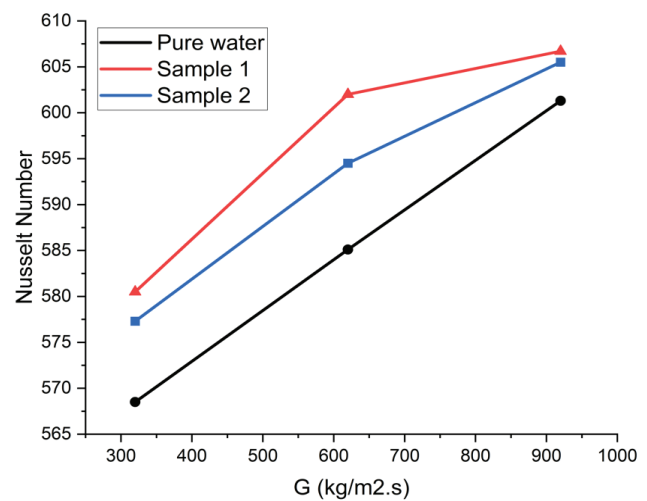
$$Nu = \frac{h_{\text{eff}} \cdot D}{k} \quad (5)$$

where  $h_{\text{eff}}$  is the effective heat transfer coefficient (W/m<sup>2</sup>K),  $D$  is the characteristic diameter (usually the tube diameter) ( $D$ ), and  $k$  is the thermal conductivity of the fluid (W/mK) [17].

The analysis of the Nusselt number ( $Nu$ ) for Sample 1 and Sample 2 in comparison to pure water reveals significant improvements in heat transfer performance due to the addition of Fe<sub>3</sub>O<sub>4</sub> nanoparticles (Fig. 10). For Sample 1, the Nusselt number increased from 580.8 at a mass flux of 320 kg/m<sup>2</sup>s to 606.7 at 920 kg/m<sup>2</sup>s, while Sample 2 showed a rise from 577.3 to 605.4 over the same range. On the other hand, pure water had lower Nusselt numbers, between 568.5 and 601.3, under the same conditions. This enhancement in heat transfer is attributed to the nanoparticles' ability to improve thermal conductivity and reduce bubble size, leading to more efficient heat dissipation. Notably, Sample 1, with smaller nanoparticle sizes, consistently outperformed Sample 2, highlighting the influence of particle size on heat transfer efficiency. These results prove that the incorporation of Fe<sub>3</sub>O<sub>4</sub> nanoparticles significantly enhances heat transfer, making nanofluids a promising solution for improving the performance of thermal systems.



**Figure 9.** Effective heat transfer coefficient vs. mass flux for pure water, samples 1 and 2.



**Figure 10.** Nusselt number vs. mass flux for pure water, samples 1 and 2.



## CONCLUSION

In this study,  $\text{Fe}_3\text{O}_4$  nanoparticles were successfully synthesized via co-precipitation with precise control over size and distribution, yielding two distinct samples: Sample 1 (29.42 nm,  $\text{NH}_4\text{OH}$ ) and Sample 2 (38.04 nm,  $\text{NaOH}$ ). Comprehensive characterization using XRD, SEM, and TEM confirmed the cubic spinel structure, spherical morphology, and high crystallinity ( $\text{CI} > 92\%$ ) of the nanoparticles. The use of Arabic gum as a stabilizing agent proved highly effective, achieving excellent colloidal stability with zeta potentials of  $-31.7$  mV and  $-35.2$  mV for Samples 1 and 2, respectively.

Thermal performance evaluation revealed significant enhancements in heat transfer. At  $620 \text{ kg/m}^2\text{s}$ , Sample 1 nanofluids exhibited a 2.7% increase in CHF compared to pure water, outperforming Sample 2 (1.6% improvement). This size-dependent enhancement is attributed to three synergistic mechanisms: (1) superior thermal conductivity due to increased phonon transport in smaller nanoparticles, (2) improved surface wettability (contact angle reduction from  $68^\circ$  to  $54^\circ$ ), and (3) formation of porous nanoparticle deposition layers on heating surfaces. The heat transfer coefficient increased by up to 28% for Sample 1 at  $920 \text{ kg/m}^2\text{s}$ , with consistent improvements in Nusselt number across all tested mass fluxes.

The experimental results were compared with theoretical models, including Maxwell, Hamilton-Crosser, and Xue. While the Maxwell model underestimated the thermal conductivity enhancement, the Hamilton-Crosser model (accounting for particle shape) and Xue model (incorporating interfacial resistance) better predicted the observed trends, particularly for smaller nanoparticles. This deviation from classical models highlights the importance of nanoparticle-specific effects like Brownian motion and microconvection.

Despite these advancements, limitations exist. The study focused on a limited range of mass fluxes (up to  $920 \text{ kg/m}^2\text{s}$ ) and a single nanoparticle concentration (0.01 wt%). Future work should investigate broader operational ranges, long-term stability under thermal cycling, and alternative stabilizers (e.g., surfactants, polymers). Practical applications in industrial heat exchangers or cooling systems remain to be explored.

These findings underscore the potential of  $\text{Fe}_3\text{O}_4$  nanofluids for thermal management applications, particularly where small efficiency gains yield significant energy savings. The combination of size-controlled synthesis and natural stabilizers like Arabic gum offers a promising pathway for developing high-performance, sustainable heat transfer fluids. Based on the findings of this research and recent studies, it is suggested that future investigations focus on optimizing hybrid nanofluids (combining  $\text{Fe}_3\text{O}_4$  with carbon nanotubes or  $\text{TiO}_2$ ) using green methods similar to [52], as well as controlling nanoparticle clustering to enhance thermal conductivity [53]. Examining the effect

of magnetic fields on heat transfer and entropy generation using advanced numerical methods [54], along with stabilizing nanoparticles under harsh conditions (such as saline environments) inspired by natural stabilization approaches like ascorbic acid [55], could provide more practical solutions for industrial applications. Combining these strategies with low nanoparticle concentrations (0.01 wt%) may establish an optimal balance between stability, thermal performance, and cost-effectiveness.

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## AUTHORSHIP CONTRIBUTIONS

Authors equally contributed to this work.

## DATA AVAILABILITY STATEMENT

Authors confirm that the data that supports the findings of this study are available within the article. The raw data that supports the findings of this study are available from the corresponding author, upon reasonable request.

## CONFLICT OF INTEREST

The authors declare no potential conflicts of interest with respect to the research, authorship, and/or publication of this article.

## ETHICS

There are no ethical issues with the publication of this manuscript.

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